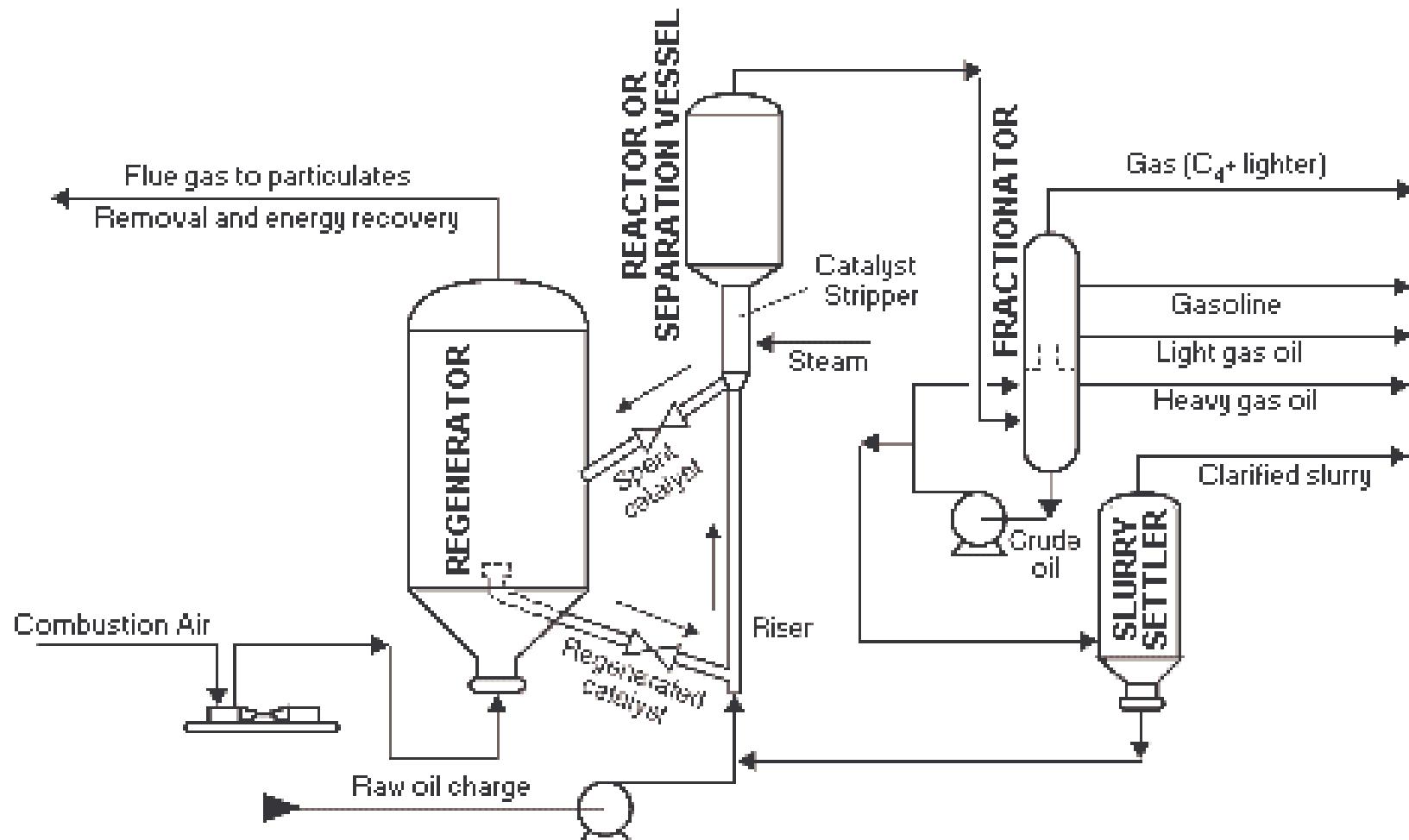


Application: Fluid Catalytic Cracker (FCC)



Reactor model

$$S_c H_{ra} \dot{T}_{ra} = S_c R_c (T_{rg} - T_{ra}) + S_{tf} R_{tf} (T_{tf} - T_{ra}) - \Delta H_{fv} R_{tf} - \Delta H_{cr} R_{tf} C_{tf}$$

$$C_{tf} = \frac{1}{1 + \frac{R_{tf}}{R_{cr}}} \quad R_{cr} = K_{cr} P_{ra} H_{ra}$$

$$C_{cat}^2 = \frac{100 P_{ra} H_{ra}}{R_c C_{rc}^{0.06}} k_{cc} \exp\left(-\frac{A_{cc}}{RT_{ra}}\right) \quad K_{cr} = \frac{k_{cr}}{C_{cat} C_{rc}^{0.15}} \exp\left(-\frac{A_{cr}}{RT_{ra}}\right)$$

$$H_{ra} \dot{C}_{sc} = R_c (C_{rc} - C_{sc}) + R_{cf}$$

$$R_{cf} = R_{cc} + R_{ad} \quad R_{ad} = F_{cf} R_{tf} \quad R_{cc} = K_{cc} P_{ra} H_{ra}$$

$$K_{cc} = \frac{k_{cc}}{C_{cat} C_{rc}^{0.06}} \exp\left(-\frac{A_{cc}}{RT_{ra}}\right)$$

Regenerator model

$$S_c H_{rg} \dot{T}_{rg} = S_c R_c (T_{ra} - T_{rg}) + S_a R_{ai} (T_{ai} - T_{rg}) + \Delta H_{rg} R_{cb}$$

$$R_{cb} = \frac{R_{ai}}{242} (21 - O_{fg}) \quad O_{fg} = 21 \exp \left(\frac{-\frac{P_{rg} H_{rg}}{R_{ai}}}{\frac{1}{K_{od}} + \frac{1}{K_{or} C_{rc}}} \right)$$

K_{or} = unknown function of T_{rg} .

$$K_{od} = 6.34 \cdot 10^{-9} R_{ai}^2$$

$$H_{rg} \dot{C}_{rc} = R_c (C_{sc} - C_{rc}) - R_{cb}$$

New form of the system

$$\begin{aligned}\varphi(x; u) &= \varphi\left(Trg, Tra, Crc, Csc, Fcf; R_{ai}\right) \\ &= \left(Trg, Tra, C_{tf}(Crc, Tra), \frac{Csc}{Crc}, \frac{Fcf}{Crc}\right) = \xi\end{aligned}$$

$$\left\{ \begin{array}{lcl} \dot{x}_1 & = & \dot{T}_{rg} = \psi(x, \varphi(x_1), u) \\ \dot{x}_2 & = & \dot{T}_{ra} = a_3(t)x_3 + f_2(x_1, x_2) \\ \dot{x}_3 & \simeq & \dot{C}_{rc} = a_4(t)x_4 \\ & & + f_3(x_1, x_2, x_3, \psi(x, \varphi(x_1), u), u, \dot{u}) \\ \dot{x}_4 & \simeq & \dot{C}_{sc} = a_5(t)x_5 + f_4(x_1, x_2, x_3, x_4) \\ \dot{x}_5 & \simeq & \dot{F}_{cf} = F(x) \end{array} \right.$$

Type 2

Here, $\psi = R_{cb}$, $\varphi = K_{or}$ and $\pi(x) = Trg = x_1$.
 $u = (R_{ai}, Pra)$

Time dependant change of coordinates

$$\frac{dx}{dt} = F(x, u)$$

Our diffeomorphism $\xi = \varphi(x, u)$ depend on u supposed to be smooth, hence:

$$\begin{aligned}\frac{d\xi}{dt} &= D\varphi(\varphi_u^{-1}(\xi)) f(\varphi_u^{-1}(\xi), u) + \frac{\partial \varphi(\varphi_u^{-1}(\xi), u)}{\partial u} \dot{u} \\ &= F(\xi, u, \dot{u})\end{aligned}$$

$$\begin{cases} \frac{d\hat{\xi}}{dt} = F(\hat{\xi}, u, \dot{u}) + PC^T R^{-1}(y - C\hat{\xi}) \\ \frac{dP}{dt} = F^*(\hat{\xi}, u, \dot{u}) P + PF^*(\hat{\xi}, u, \dot{u}) + Q_\theta - PC^T R^{-1} CP \end{cases}$$

In the original coordinates

Since $C\varphi_u(x) = Cx$, equations are those of a modified extended Kalman filter

$$\left\{ \begin{array}{l} \frac{d\hat{x}}{dt} = f(\hat{x}, u) + pC^T R^{-1} (y - C\hat{x}) \\ \frac{dp}{dt} = f^*(\hat{x}, u)p + pf^*(\hat{x}, u)^T + q_\theta(\hat{x}) \\ \quad - ph^*(\hat{x}, u)^T R^{-1} h^*(\hat{x}, u)p \\ \quad + D_{\psi_u}^{-1}(\hat{x}) D_{\psi_u}^2 \cdot \left(ph^*(\hat{x}, u)^T R^{-1} (h(\hat{x}, u) - y) \right) p \\ \quad + p D_{\psi_u}^2 \cdot \left(ph^*(\hat{x}, u)^T R^{-1} (h(\hat{x}, u) - y) \right) D_{\psi_u}^{-1}(\hat{x})^T \end{array} \right.$$

where $q_\theta(\hat{x}) = D_{\varphi_u}(\hat{x})^{-1} Q_\theta \left(D_{\varphi_u}(\hat{x})^{-1} \right)^T$

The two last lines (transposed) correspond to the change of coordinate.

Tuning

We use a second order system to estimate K_{or}

i.e. $\frac{d^3 K_{or}}{dt^3} = 0$

We use three parallel extended Kalman filters such that

- $\theta_0 = 3$ (starting value for each observers)
- $\theta_{HG} = 2$ (minimal value of θ ensuring high-gain)
- Time between two consecutive initializations: 2 hours

EKF with two outputs

At last,

$$\xi = \left(Trg, R_{cb}, \dot{K}_{or}, \ddot{K}_{or}, Tra, C_{tf}, \frac{C_{sc}}{C_{rc}}, \frac{F_{cf}}{C_{rc}} \right)$$

and

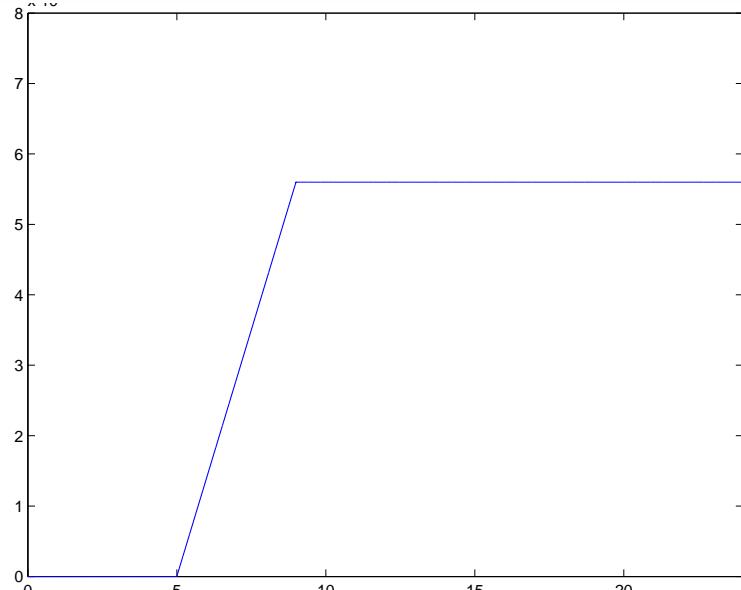
$$\Delta^{-1} = \text{diag} (1, \theta, \theta^2, \theta^3, 1, \theta, \theta^2, \theta^3)$$

$$\text{with } Q_\theta = \theta^2 \Delta^{-1} Q \Delta^{-1}$$

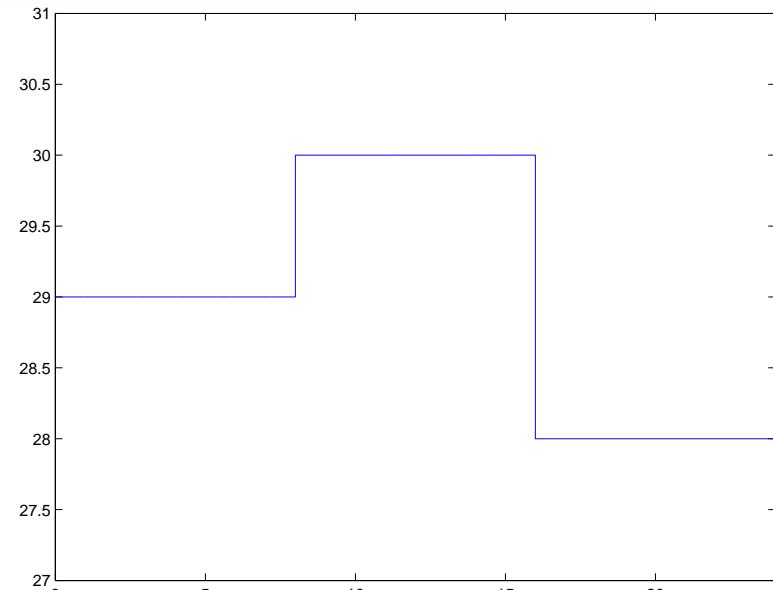
$$\text{and } R_\theta = (C \Delta^{-1} C') R (C \Delta^{-1} C')$$

Simulations

Colored noise (Ornstein–Uhlenbeck process) on both measured variables T_{rg} and T_{ra} .



Unknown parameter F_{cf}



Control variable R_{ai}

$$K_{or} = 1.16 \cdot 10^{-5} \exp \left(\frac{A_{or}}{R \left(\frac{1}{866.7} - \frac{1}{T_{rg}} \right)} \right)$$

Constants of the model

Reactor operating conditions

$$H_{ra} = 1.85 \cdot 10^{-4}, P_{ra} = 211.7,$$

Feed properties

$$R_{tf} = 41, T_{tf} = 492.8, S_{tf} = 3140,$$

Cat.recirculation

$$R_c = 290, S_c = 1047,$$

Heat constants

$$\Delta H_{cr} = 4.65 \cdot 10^5, \Delta H_{fv} = 1.74 \cdot 10^5,$$

$$\Delta H_{rg} = 3.02 \cdot 10^7, R = 8.314$$

$$k_{cr} = 8.31 \cdot 10^{-2}, A_{cr} = 6.28 \cdot 10^4,$$

$$k_{cc} = 2.66 \cdot 10^{-4}, A_{cc} = 4.18 \cdot 10^4$$

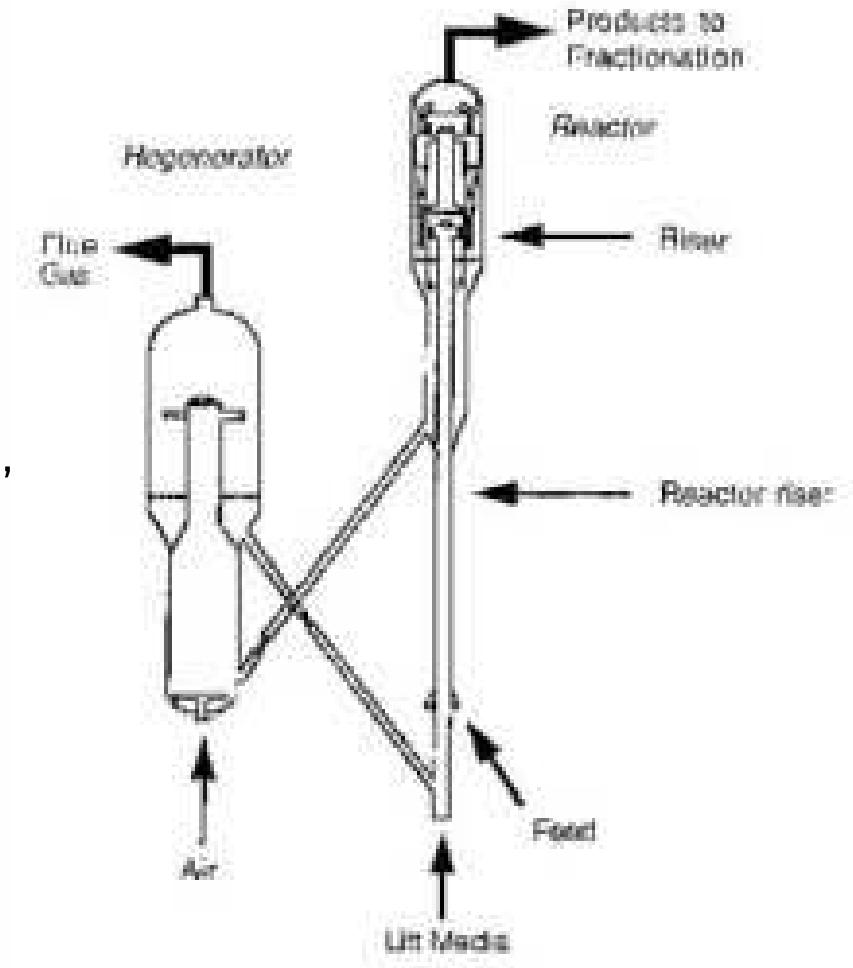
Regenerator operating conditions

$$H_{rg} = 1.53 \cdot 10^5, P_{rg} = 254.4,$$

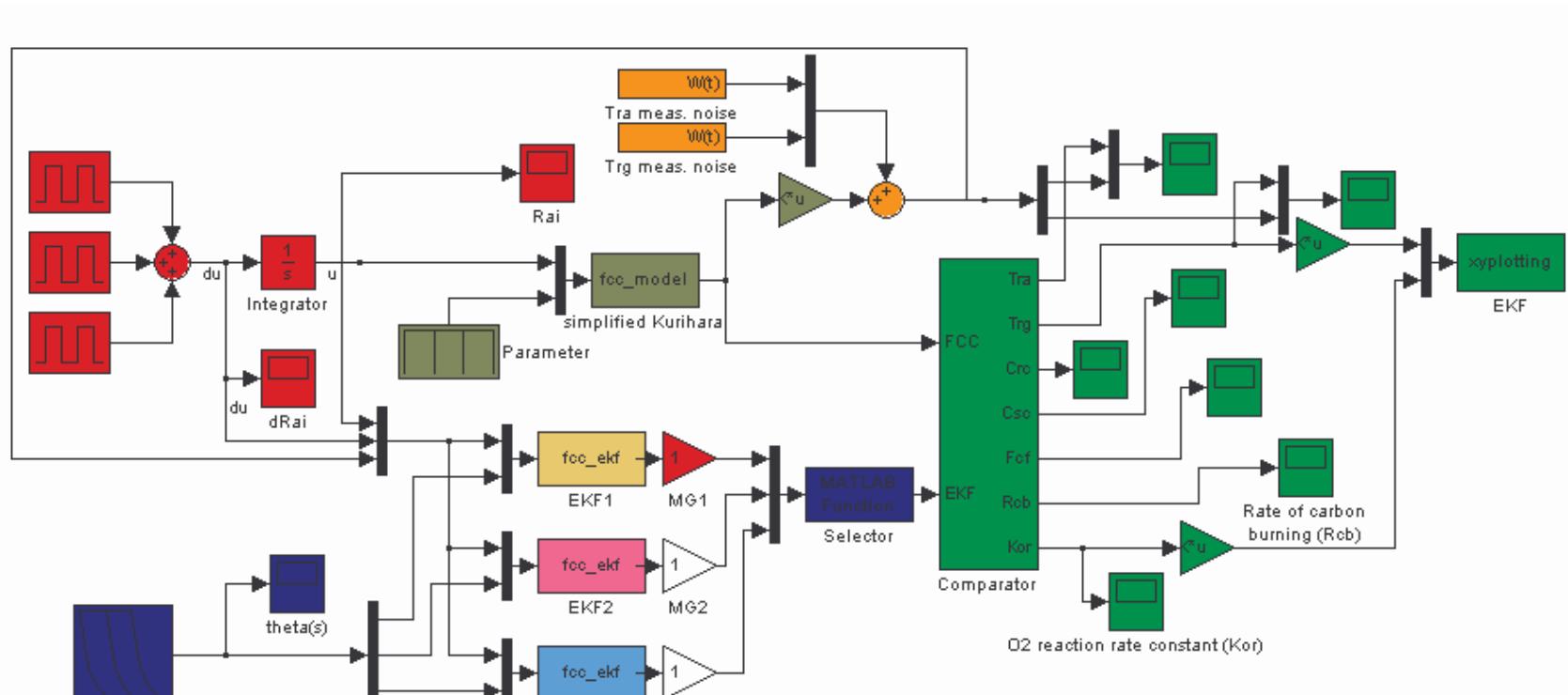
Air properties

$$R_{ai} = 26, T_{ai} = 394, S_{ai} = 1130$$

$$A_{or} = 1.47 \cdot 10^5$$

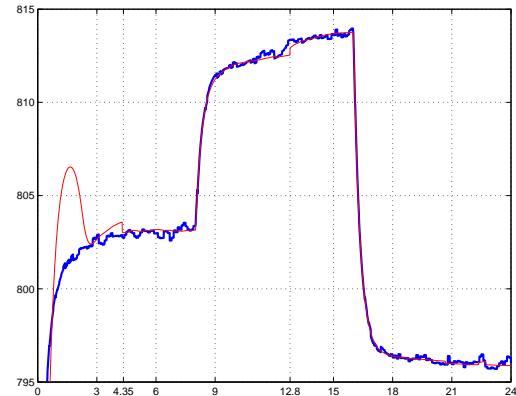


Simulation using Matlab/Simulink



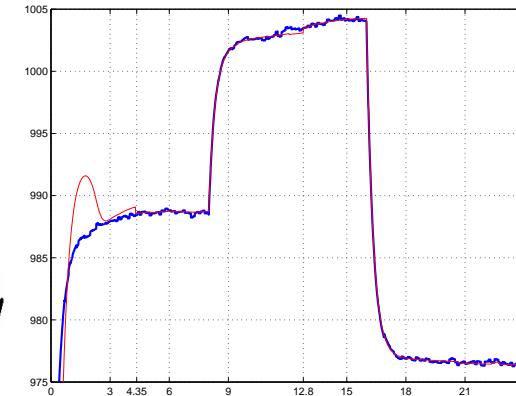
to be continued...

Observer: State estimation



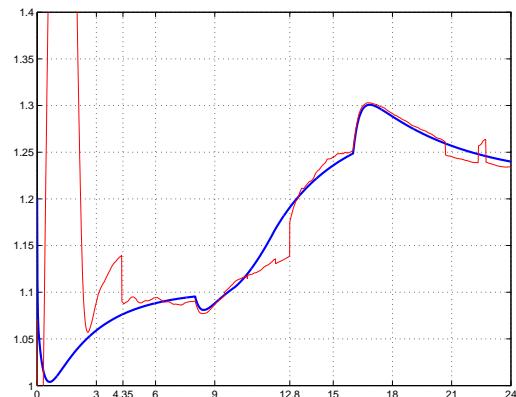
T_{ra}

Reactor

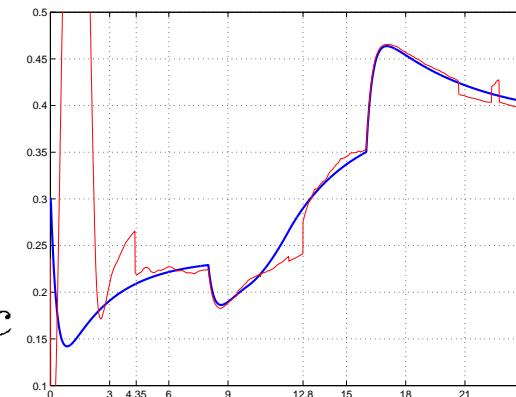


T_{rg}

Regenerator



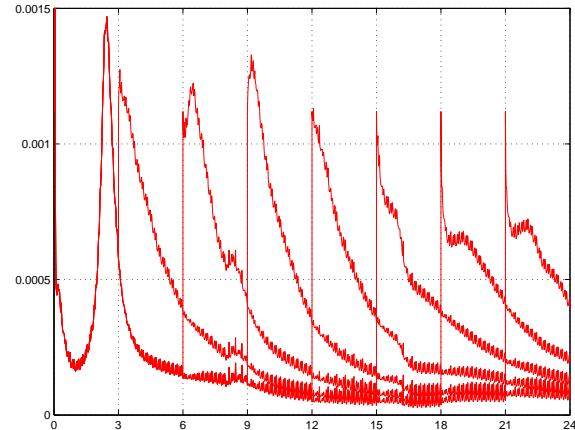
C_{scc}



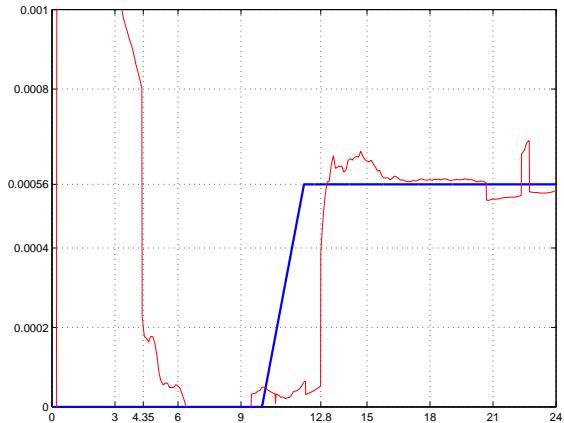
C_{rc}

— actual process
— observer

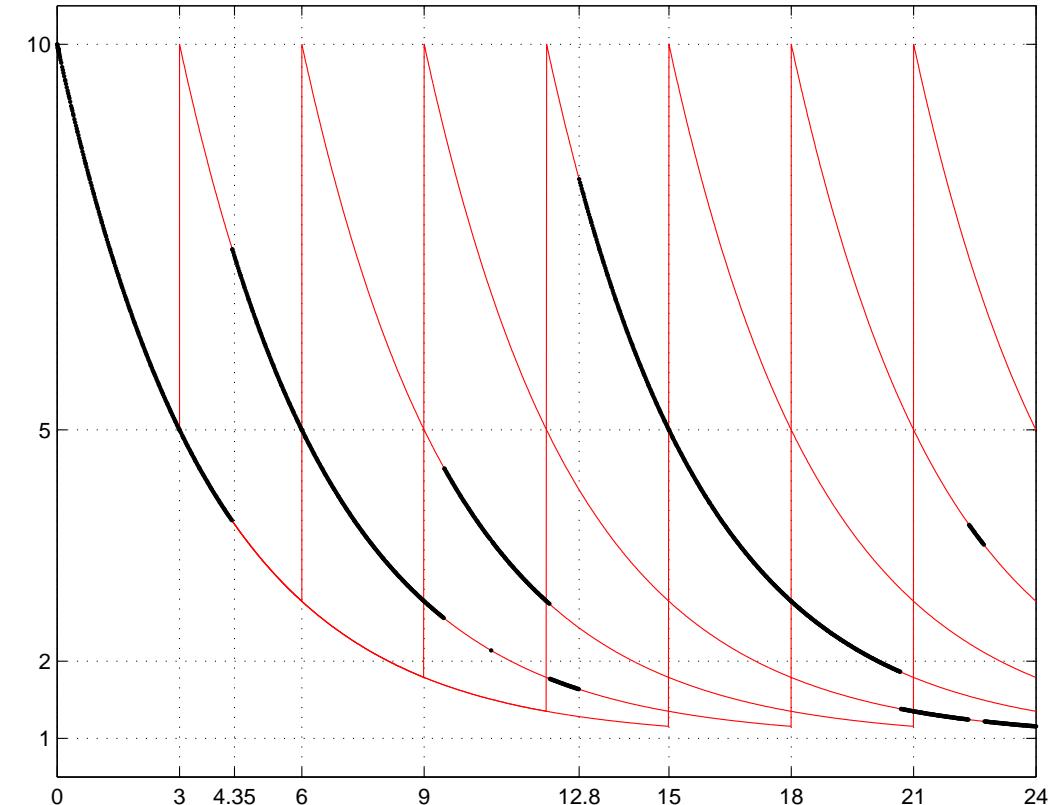
Observer: Parameter estimation



Norm of the gain

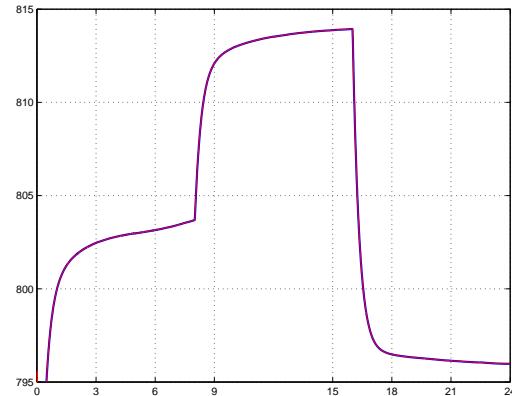


F_{cf}



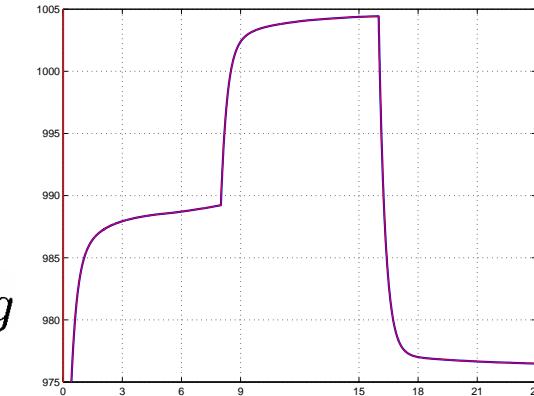
— actual process
— observer

Identification: state estimation



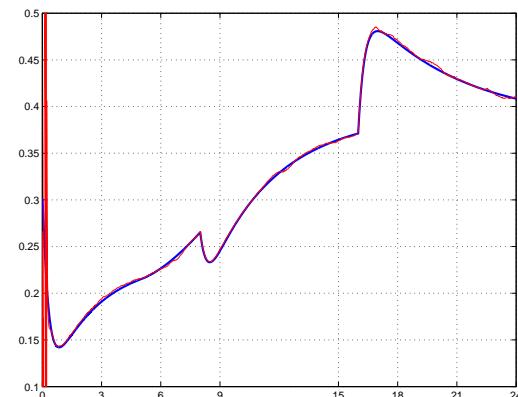
T_{ra}

Reactor

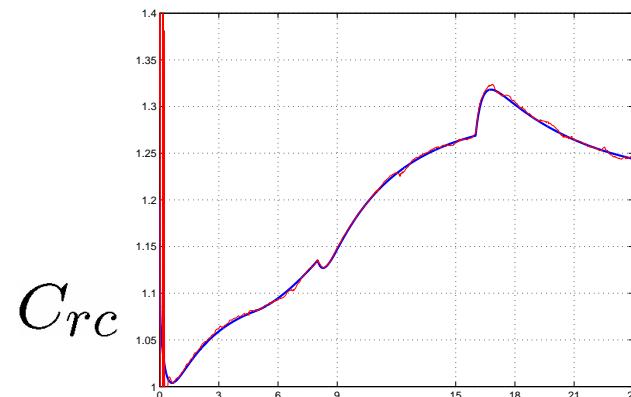


T_{rg}

Regenerator



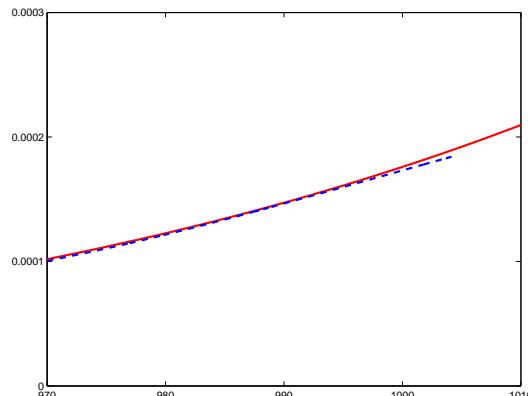
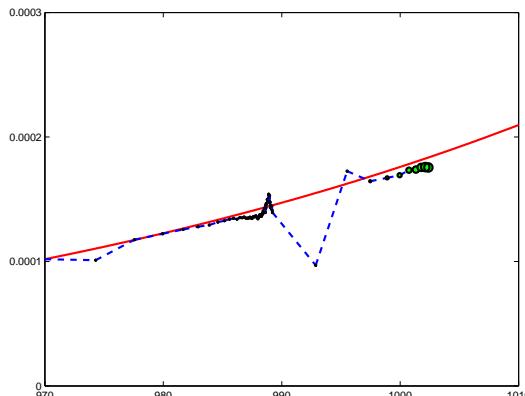
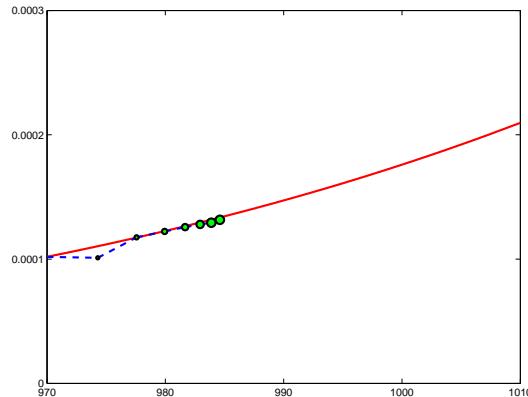
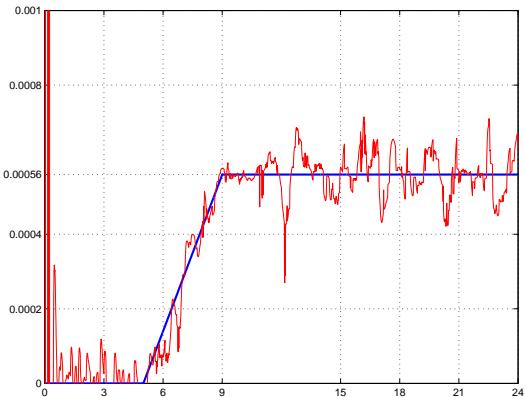
C_{sc}



C_{rc}

	actual process
	observer

Identification of unknown function



— actual process
— observer